

# Molybdate-based double perovskite materials in methane dry reforming

Thomas F. Winterstein<sup>a,1</sup>, Christoph Malleier<sup>a,1</sup>, Bernhard Klötzer<sup>a</sup>, Volker Kahlenberg<sup>b</sup>, Clivia Hejny<sup>b</sup>, Maged F. Bekheet<sup>c</sup>, Julian T. Müller<sup>c</sup>, Aleksander Gurlo<sup>c</sup>, Marc Heggen<sup>d</sup>, Simon Penner<sup>a,\*</sup>

<sup>a</sup> Institute of Physical Chemistry, University of Innsbruck, Innrain 52c, A-6020, Innsbruck, Austria

<sup>b</sup> Institute for Mineralogy and Petrography, University of Innsbruck, Innrain 52d, A-6020, Innsbruck, Austria

<sup>c</sup> Technische Universität Berlin, Faculty III Process Sciences, Institute of Materials Science and Technology, Chair of Advanced Ceramic Materials, Straße des 17. Juni 135, 10623, Berlin, Germany

<sup>d</sup> Ernst Ruska-Centre for Microscopy and Spectroscopy with Electrons, Forschungszentrum Jülich GmbH, Leo-Brandt-Str. 1, D-52428, Jülich, Germany

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## ABSTRACT

A series of  $\text{Sr}_2\text{MMoO}_6$  ( $M = \text{Ni, Co and (Ni,Co)}$ ) compounds was tested as representative model systems to highlight the capabilities of double perovskite structures as precursor materials for methane dry reforming (DRM) applications. Pretreatments in either pure hydrogen or dry reforming  $\text{CO}_2/\text{CH}_4$  mixtures exclusively yield partial decomposition of the initial double perovskite structures through exsolution of small Ni or CoO particles and the associated formation of additional crystalline compounds, such as  $\text{SrMoO}_4$  or  $\text{SrCO}_3$  (in DRM mixtures). The formation of a defective  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  transient phase has been revealed by in situ X-ray diffraction measurements in a pure hydrogen atmosphere. The main difference between the Ni- and Co-containing Sr molybdate perovskite structures is the much stronger oxidation propensity of exsolved Co, most likely by oxygen supply from the partially intact double perovskite structure. For  $\text{Sr}_2\text{NiMoO}_6$ , the resulting metallic Ni-double perovskite interface is highly DRM active without strong coking, both if a pre-reduction step in hydrogen is carried out before the DRM experiment or if  $\text{Sr}_2\text{NiMoO}_6$  is directly decomposed in the DRM mixture. Despite partial decomposition, the corresponding  $\text{Sr}_2\text{CoMoO}_6$  structure is not active under DRM operation, most likely due to the in situ formation of small exsolved CoO particles, while Ni is exsolved in its metallic state. Different strategies to improve the catalytic activity, including hydrogen by-mixing, enhanced A-site deficiency or co-alloying with Ni have been followed, but only the latter has a beneficial effect on improving the DRM activity at compositions of  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ . In  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ , the substitution of Co by Ni suppresses the oxidation propensity of Co and during DRM yields the exsolution of Co-rich Ni-Co alloy nanoparticles. We also reveal a strong response of molybdenum as the B' site cation to reduction and DRM treatment, causing the formation of reduced  $\text{MoO}_x$  phases accompanying the exsolution process.

## 1. Introduction

The dry reforming of methane (DRM) reaction is a viable way to convert two anthropogenic greenhouse gases, carbon dioxide ( $\text{CO}_2$ ) and methane ( $\text{CH}_4$ ), into a carbon monoxide (CO) and hydrogen ( $\text{H}_2$ ) mixture (so-called “syngas”). The latter can be used as a valuable feedstock for the production of a wide array of synthetic chemicals, including Fischer-Tropsch products, aldehydes or alcohols [1]. The DRM reaction (equation (1)) is highly endothermic ( $\Delta H^\circ_{298} = 247.3 \text{ kJ mol}^{-1}$ ), which requires operation at elevated temperatures,

typically between 600 °C–1000 °C [1].

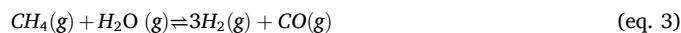
Methane Dry Reforming:



Reverse Water Gas Shift reaction:



Steam Reforming of Methane:



\* Corresponding author.

E-mail address: [simon.penner@uibk.ac.at](mailto:simon.penner@uibk.ac.at) (S. Penner).

<sup>1</sup> These two authors contributed equally.

Boudouard reaction:



Methane decomposition:



The DRM reaction represented by eq. (1) is only the main reaction, which is accompanied by a plethora of side reactions, including methane decomposition, methane steam reforming, Boudouard reaction and/or the water-gas shift equilibrium (eqs. (2)–(5)). All of these reactions are critical for catalyst coking, regeneration, and activity/selectivity [1,2]. The archetypical, most widely used catalyst material is Ni metal. It offers very high activity in both carbon dioxide and methane activation, but suffers from the severe drawback of sintering of the active metal particles and surface/bulk deactivation by coke deposition [3]. To overcome this issue materials-wise, a number of material classes, e.g., complex oxides [2,4] or intermetallic compounds [4,5] have been successfully screened. In many cases, the studied catalyst entities rival or even outperform the archetypical materials in terms of catalyst stability, suppression of coke formation or catalyst activity [1–5]. A particularly promising class of materials is perovskites, which feature the general formula  $\text{ABX}_3$ , where X is usually a halide or oxygen and A and B are typically bi- or trivalent ions occupying the dodecahedrally and octahedrally coordinated sites. Typical A site ions are earth-alkaline metal ions (e.g.,  $\text{Sr}^{2+}$  or  $\text{Ca}^{2+}$ ) or other large cations such as  $\text{La}^{3+}$ . The B site ions are usually transition metal ions [2]. The huge advantage of perovskites is the possibility to tune the structural and physico-chemical properties of the materials by an adequate choice of the A- and B-site ions [2]. This likewise affects the oxygen vacancy concentration/oxygen mobility, structural stability or catalytic activity/selectivity [2]. These beneficial properties also hold for so-called double perovskite structures, which are characterized by the general formula  $\text{AA}'\text{BB}'\text{O}_6$ . The characteristics of this class of materials are the appearance of different possibilities of B-site cation ordering, such as rock-salt, layered or columnar [6]. The ordering phenomena directly affects the crystal chemistry of the materials and the possibility of valence mixing at the B/B' site gives rise to an even more pronounced tuning of catalytic, structural or electronic properties. Consequently, double perovskites can be formed by successive substitution of A' for A and/or B' for B. This initially leads to a doped single perovskite  $\text{A}_{1-x}\text{A}'_x\text{BO}_3$  (or  $\text{AB}_{1-y}\text{B}'_y\text{O}_3$ ), where in general, the cations adopt a disordered structure through random occupation of the A- or B-sites. If A and A' (or B' and B) differ significantly in size or charge, and x (or y) is approximately equal to 0.5, ordered double perovskites may be formed. It is worth noting that the important benefits are significantly improved compared to their single perovskite counterparts. These include (i) the expansion of the compositional space because double perovskite structures may accommodate elements/ions that cannot exist in standard perovskites (e.g., high valence states +6 or +7), (ii) the complex atomic coordination can lead to electronic structures not found in standard perovskites and (iii) double perovskites can exhibit a higher chemical stability, e.g., in highly reducing or oxidizing environments [7].

The use of (double) perovskites in the DRM reaction is usually connected to the exploitation of perovskite structures as precursors, which are decomposed in a controlled manner to result in well-distributed metal nanoparticles embedded in an oxide matrix. The formation of the metal-oxide interface gives rise to a bifunctional catalytic mechanism, in which the metal (methane activation) and oxide (carbon dioxide activation) share duties. This mechanism is prevalent in the most studied  $\text{LaNiO}_3$  and  $\text{La}_2\text{NiO}_4$  materials, where  $\text{La}_2\text{O}_2\text{CO}_3$  (as a result of perovskite decomposition towards  $\text{La}_2\text{O}_3$ ) is reversibly formed and decomposed by  $\text{CO}_2$  activation and release [8,9]. Recent studies have also shown that even interfacial carbides can act as a reactive intermediate [10,11]. This interface features higher structural and sinter stability with enhanced catalytic activity and suppressed carbon deposition. Perovskite decomposition necessarily goes along with the

exsolution of metal particles from the (double) perovskite lattice and is such a common phenomenon [12,13]. It is usually induced by a separate pre-reduction step (mostly in hydrogen) or “in situ” in the reaction mixture itself. While the exsolution of metals from several single perovskites, especially for DRM applications, has already been scrutinized especially for DRM applications [5,8,14–16], much less information is available for double perovskites as starting precursors. To date, research on double perovskites has focused primarily on the exsolution of iron, iron-nickel, and cobalt-iron alloy particles from (cobalt-doped)  $\text{Sr}_2\text{Fe}_{1-x}\text{Mo}_x\text{O}_6$  and  $\text{Sr}_2\text{Ni}_x\text{Fe}_{1-x}\text{O}_6$  materials [17–25]. A composition-dependent  $\text{FeNi}_3$  exsolution, correlated with increased  $\text{CO}_2$  and  $\text{CH}_4$  conversion, has been found. Molybdate-based double perovskites with Sr on the A site exhibit especially excellent exsolution properties [17]. The formation of a  $\text{Mo}^{6+}/\text{Mo}^{5+}$  redox couple upon reduction is of particular importance in the context of DRM applications, specifically in the case of  $\text{Sr}_2\text{NiMoO}_6$  and  $\text{Sr}_2\text{CoMoO}_6$ . This redox couple enhances the dissociative chemisorption of methane, which is a crucial step in the overall process. In due course, the formation of  $\text{Mo}=\text{O}$  species is reported to favor the reaction of methane with a surface ion by lowering its acidity and desorption energy for the oxidized reaction product [26].

It is noteworthy that, despite the information that has been compiled so far, ex situ post-mortem catalyst characterization is typically the only available data for such double perovskites in DRM. This represents a significant limitation, as analogous studies on single perovskites, particularly pure and doped  $\text{LaNiO}_3$ , have demonstrated that the characterization of the spent catalyst state is insufficient to draw definitive conclusions about the active site. Structural transformations occurring during DRM operation tremendously influence the catalytic properties, and include the formation of oxygen-deficient phases, Ruddlesden-Popper phases or oxy-carbonates [8]. The objective of the present study is to examine the reductive stability and associated DRM properties of two “model” double perovskite structures,  $\text{Sr}_2\text{NiMoO}_6$  and  $\text{Sr}_2\text{CoMoO}_6$ . Both double perovskite structures have been selected, as the corresponding Ni- and Co-containing perovskites have already shown prospective methane activation and DRM properties [8,15]. The use of Ni- and Co-based double perovskites on molybdate basis also allows us to eventually connect the exsolution properties of the B-site ion (Ni, Co) with possible changes in the electronic structure and oxidation state of the B' ion (Mo) and their effects on DRM activity. In due course, we will compare the eventual transition of the double perovskite precursor structure into the metal/oxide/perovskite composite in hydrogen and in the DRM reaction mixture, as for single perovskites, distinct differences in the observed transient structures and Ni particle sizes have already been obtained. The cross-correlation of the Ni- and Co results will yield similarities and differences in the stability, decomposition route, carbon resistance, and oxidation behavior of the exsolved metal particles in double perovskite. Additionally, activation strategies for selected  $\text{Sr}_2\text{CoMoO}_6$  materials, including A-site deficiency and co-alloying of Co with Ni, will be discussed.

## 2. Experimental

### 2.1. Synthesis of $\text{Sr}_2\text{NiMoO}_6$ , $\text{Sr}_2\text{CoMoO}_6$ , $\text{Sr}_2\text{Ni}_x\text{Co}_{1-x}\text{MoO}_6$ and $\text{Sr}_{1.9}\text{CoMoO}_6$

For synthesis of the double perovskite materials  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{CoMoO}_6$ ,  $\text{Sr}_2\text{Ni}_{0.1}\text{Co}_{0.9}\text{MoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  and  $\text{Sr}_{1.9}\text{CoMoO}_6$  we followed a solid-state preparation route, which includes mechanically mixing the starting materials  $\text{SrCO}_3$  (Sigma-Aldrich, 99.9 % trace metals basis),  $\text{Co}_3\text{O}_4$  (Thermo Fisher, 99.7 % metals basis),  $\text{NiO}$  (Thermo Fisher, Puratronic 99.998 % metals basis) and  $\text{MoO}_3$  (Thermo Fisher, 99.95 % metals basis) in the respective nominal stoichiometries followed by grinding and homogenizing the powders in ethanol with an agate ball mill at 600 rpm for 45 min. After evaporation of the alcohol, the powder was calcined at 900 °C for 24 h, after which it was ground and pressed

into a pellet. The pellets were subsequently subjected to repeated sintering – grinding cycles, including heating to 1350 °C for 24 h followed by re-pelletizing into a tablet of 10 mm diameter and 0.8 mm thickness. This procedure was repeated until X-ray diffraction (XRD) indicated the lowest achievable amount of parasitic structures. The amounts used for the synthesis of 2 g material each are summarized in Table 1.

For Mo-based double perovskite structures, a very low amount of  $\text{SrMoO}_4$  (<3 wt.-%) is always observed. This compound is isotypic with zircon ( $\text{ZrSiO}_4$ ). As will be shown in this contribution, the appearance/formation and transformation into other Sr-molybdate structures are highly dynamic and strongly dependent on the gas atmosphere and treatment. The synthesis of all the compounds yielded a double perovskite structure. Fig. 1 shows a representative tetragonal crystal structure of  $\text{Sr}_2\text{NiMoO}_6$ .

## 2.2. Structural and spectroscopic characterization

Ex situ structural analysis of benchmark materials after selected treatments was carried out using a Rigaku SmartLab-SE instrument in focused beam setting and reflection mode (Co-K $\alpha$ ,  $\lambda = 1.7890 \text{ \AA}$ ) using a D/tex Ultra 250 compound silicon strip 1D-detector (Rigaku, Tokyo, Japan). The ground sample was placed on a glass-sample holder, and the patterns were recorded in a range of  $2\theta = 10^\circ\text{--}90^\circ$  with a step width of  $0.01^\circ$ .

In situ synchrotron-based PXRD experiments have been conducted on both DRM mixtures under pure hydrogen at beamline 12.2.2, Advanced Light Source (ALS) at Lawrence Berkeley National Laboratory, in a cell previously described in Refs. [29,30]. All diffraction patterns were measured in angle-dispersive transmission mode with a focussed 25 keV monochromatic beam ( $\lambda = 0.4984 \text{ \AA}/30 \text{ \mu m}$  spot size). The powders were heated in a 0.7 mm outer diameter quartz capillary under quasi-flowing conditions ( $\text{CH}_4:\text{CO}_2 = 1:1$ , gas flow:  $1 \text{ mL min}^{-1}$  for DRM; pure hydrogen, gas flow  $1 \text{ mL min}^{-1}$ , GHSV =  $600\,000 \text{ N mL h}^{-1} \text{ gcat}^{-1}$ ). Heating was performed using a SiC furnace with an infrared light source up to 800 °C at a rate of  $10^\circ \text{C min}^{-1}$ . All gases were injected through a 0.5 mm outer diameter tungsten tube [29,30]. The program TOPAS 5.0 by Bruker was utilized to analyze the X-ray diffraction patterns using Rietveld refinement with a full axial model [31]. A Double-Voigt approach was applied to calculate the crystallite sizes. The resolution function of the diffractometers was obtained from the structure refinement of a  $\text{LaB}_6$  standard.

Surface chemical analysis was carried out in a commercial UHV system for in situ XPS applications (SPECS GmbH). The UHV chamber is comprised of a  $\mu\text{FOCUS}$  600 monochromatic small spot ( $100 \times 300 \text{ \mu m}^2$ ) Al K $\alpha$  X-ray source, a hemispherical energy analyzer (PHOBIOS 150 NAP) in a vertical configuration, and a  $\mu$ -metal analyzing chamber, shielding the system from external magnetic fields. To investigate polycrystalline samples, a pressed pellet covering a stainless-steel grid as a stabilizer is fixed on a sample-holder by mounting the pellet via a front plate. The excited photo-electrons were collected by a  $300 \text{ \mu m}$  nozzle directly from the sample's frontside surface via an 8 mm opening in the front plate. Details of the apparatus are given in Ref. [32]. Qualitative analysis was based on the Ni 2p, Sr 2p, Co 2p, O 1s, C 1s and Mo 3d high-resolution spectra. Chemical shifts were calibrated to the signal of the adventitious carbon component at 284.5 eV. Fitting of the Ni 2p, Co

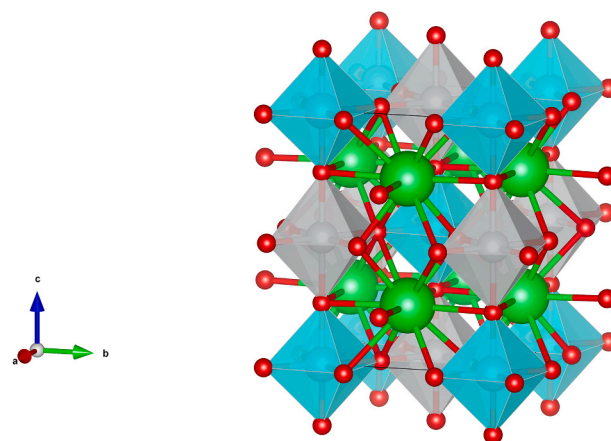


Fig. 1. Structure model of the synthesized representative tetragonal  $\text{Sr}_2\text{NiMoO}_6$  double perovskite structure. Sr is shown in green, Ni octahedrons in blue, Mo octahedrons in grey and oxygen in red. The graphical illustration was created using the program VESTA [27]. Modelled after the structure described in [28]

2p and Mo 3d spectra by different components and oxidation states was performed using literature-reported constraints for the full-width at half maximum and the binding energies. Background correction has been done using Shirley- and Tougaard-type functions.

Scanning transmission electron microscopy (TEM) characterization via high-angle annular dark field (HAADF) imaging and Energy-dispersive X-ray analysis was carried out on an  $\text{C}_s$ -aberration corrected (Ceos DCOR) FEI Titan G2 80–200 ChemiSTEM electron microscope operated at 200 kV at the Ernst Ruska-Centre Jülich employing an in-column Super-X energy dispersive X-ray spectroscopy (EDX) unit (ChemiSTEM technology)

## 2.3. Catalytic characterization

200 mg of sample powder was fixed with quartz wool in a home-built 7 mm (inner diameter) quartz tube flow reactor setup under a total continuous gas flow of  $60 \text{ mL min}^{-1}$  ( $\text{CH}_4:\text{CO}_2:\text{He} = 1:1:1 \text{ mL min}^{-1}$ ). The reactor was heated with  $5^\circ \text{C min}^{-1}$  to 800 °C, followed by an isothermal period at 800 °C for 30 min. An external S-type thermocouple was placed in close contact to the reactor tube to ensure the correct temperature reading. Moreover, an independent calibration of a potential temperature gradient between the external thermocouple and the exact location of the catalyst bed was performed by inserting a second thermocouple into the gas flowing inside the reactor tube. The output gas was directly detected by an on-line quadrupole mass spectrometer (Balzers QME 125).  $\text{CO}_2$ ,  $\text{CH}_4$ , CO and  $\text{H}_2$  were measured at their respective  $m/z$  ratios of  $m/z = 44$ , 16, 28 and 2, respectively. Relevant fragmentation patterns have been considered. For the display of the catalytic data, we show the conversion of the relevant signals as a qualitative measure of the catalytic activity, as due to the ongoing structural transformations during the DRM reaction, active-site-normalized reaction rates (and consequently, TOF values) cannot be reliably calculated.

## 3. Results and discussion

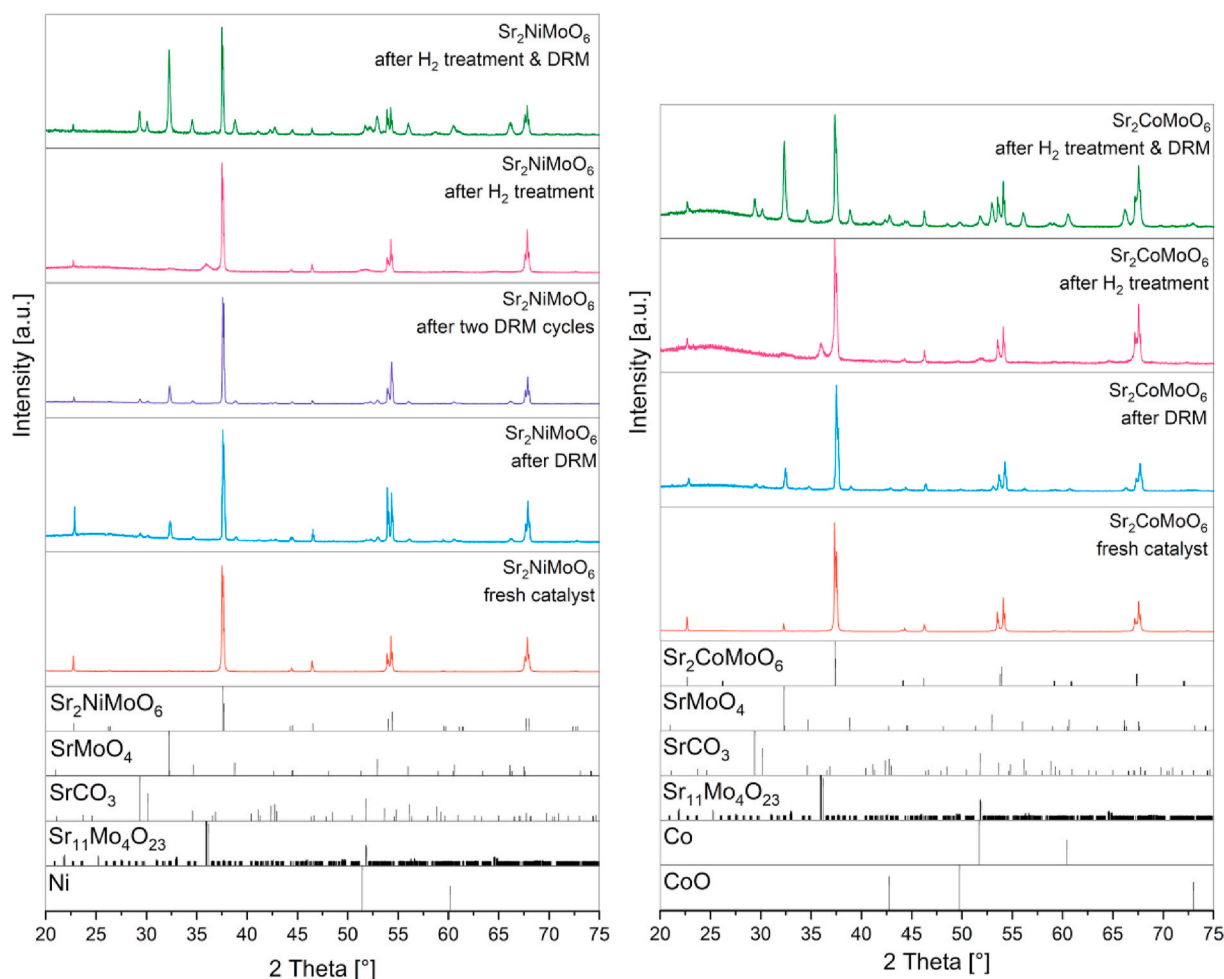
### 3.1. Bulk structure characterization of selected benchmark states of $\text{Sr}_2\text{NiMoO}_6$ , $\text{Sr}_2\text{CoMoO}_6$ and $\text{Sr}_2\text{Ni}_x\text{Co}_{1-x}\text{MoO}_6$ before and after hydrogen reduction and methane dry reforming

Figs. 2 and 3 show a combined ex situ PXRD analysis of the as-calcined and differently pre-treated  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{CoMoO}_6$  and  $\text{Sr}_2\text{Ni}_x\text{Co}_{1-x}\text{MoO}_6$  samples. These measurements serve as the basis for Rietveld analysis to confirm the presence of the double perovskite

Table 1

Stoichiometric masses of reactants used for the perovskite synthesis. The combined mass of each sample is set to 2 g.

Phase	$\text{SrCO}_3$ [g]	$\text{MoO}_3$ [g]	$\text{NiO}$ [g]	$\text{Co}_3\text{O}_4$ [g]
$\text{Sr}_2\text{NiMoO}_6$	1.1491	0.5602	0.2907	–
$\text{Sr}_2\text{CoMoO}_6$	1.1368	0.5542	–	0.3090
$\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$	1.1429	0.5572	0.1446	0.1554
$\text{Sr}_{1.9}\text{CoMoO}_6$	1.1115	0.5704	–	0.3181
$\text{Sr}_2\text{Co}_{0.9}\text{Ni}_{0.1}\text{MoO}_6$	1.1380	0.5548	0.0288	0.2784



**Fig. 2.** PXRD analysis of  $\text{Sr}_2\text{NiMoO}_6$  (Left column) and  $\text{Sr}_2\text{CoMoO}_6$  (Right column) in the as-calcined state, after pre-reduction in hydrogen at 800 °C, and after one or several DRM cycles up to 800 °C, with and without pre-reduction in hydrogen at 800 °C. Structural references are shown as bars at the bottom of the respective panels. Pattern numbers:  $\text{Sr}_2\text{NiMoO}_6$  155732 [28],  $\text{Sr}_2\text{CoMoO}_6$  181514 [33],  $\text{SrMoO}_4$  2300460 [34],  $\text{SrCO}_3$  9013802 [35],  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  143701 [36], Ni 37502 [37], Co 136039 [38], CoO 9865 [39]. Parameters: Hydrogen or DRM atmosphere ( $\text{CO}_2:\text{CH}_4:\text{He} = 1:1:1$ ), flow rate: 60 mL min<sup>-1</sup>, heating rate: 5 °C min<sup>-1</sup>.

structure and structural benchmarks after different treatments that form the basis of the stability tests discussed in the subsequent section. We were able to synthesize all materials as tetragonal double perovskites with only minor differences in the unit-cell parameters (Table 2).  $\text{SrMoO}_4$  as the common parasitic phase is present in very low concentrations (i.e., <3 wt.-% for  $\text{Sr}_2\text{CoMoO}_6$ , <2 wt.-% for  $\text{Sr}_2\text{NiMoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  materials). An exception is the  $\text{Sr}_2\text{Ni}_{0.1}\text{Co}_{0.9}\text{MoO}_6$  sample, which also contains a small  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  impurity.

The morphology and chemical homogeneity of all samples were determined by electron microscopy analysis. Fig. 4 shows the results for the calcined  $\text{Sr}_2\text{NiMoO}_6$  (Panel A) and the  $\text{Sr}_2\text{Co}_{0.5}\text{Ni}_{0.5}\text{MoO}_6$  (Panel B) samples. In both cases, HAADF images reveal a platelet-like morphology with individual plate sizes of several hundreds of nm. Most importantly, the EDX analysis shows that all elements are homogeneously distributed and no agglomeration of any element occurred.

### 3.2. Stability of $\text{Sr}_2\text{NiMoO}_6$ and $\text{Sr}_2\text{CoMoO}_6$ under reduction and methane dry reforming conditions

#### 3.2.1. Structural benchmark states after hydrogen reduction and DRM treatment

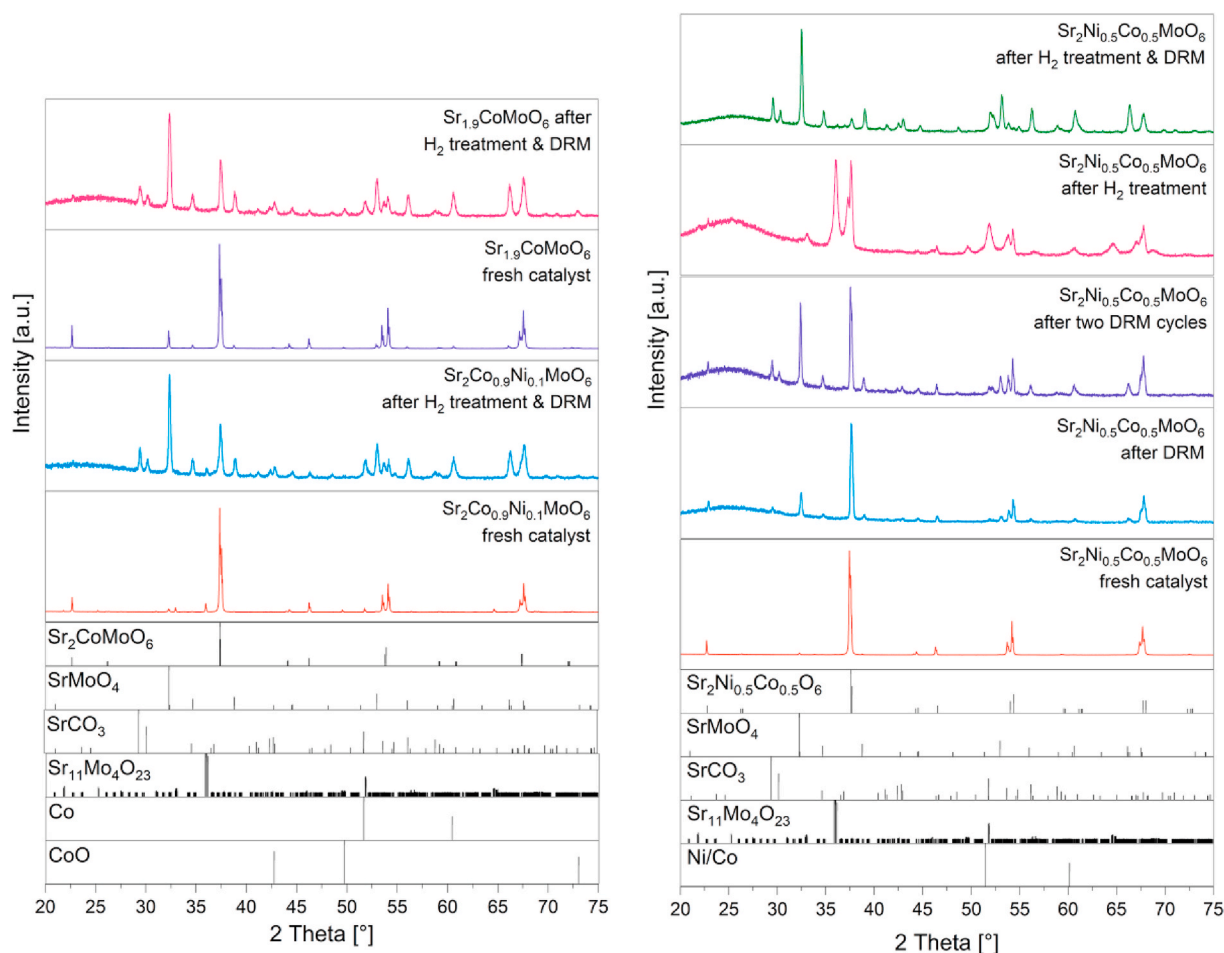
With respect to stability,  $\text{Sr}_2\text{NiMoO}_6$  was already tested in literature [26,40–42] and, although there are contradictory reports on the extent of decomposition, there is common agreement that upon heating in hydrogen/inert gas mixtures, partial or complete decomposition has

been observed. Heating in a 5 %  $\text{H}_2/\text{N}_2$  mixture at 1200 °C yielded exsolution of Ni particles from the double perovskite lattice, essentially resulting in a Ni metal - double perovskite interface with Sr-molybdate parasitic structures [26]. In contrast, heating in 5 %  $\text{H}_2/\text{Ar}$  at 1200 °C yielded complete decomposition into Ni,  $\text{Sr}_3\text{MoO}_6$ ,  $\text{SrMoO}_3$  and  $\text{SrMoO}_4$  [26]. The latter phase is a common product of the decomposition of Sr–Mo perovskite phases [43]. Of equal importance for DRM applications,  $\text{Sr}_2\text{NiMoO}_6$  yields partial decomposition into  $\text{SrCO}_3$ , Ni and  $\text{SrMoO}_4$  in pure  $\text{CO}_2$  starting at 600 °C. Ni particles exsolved from  $\text{Sr}_2\text{NiMoO}_6$  are reported to be highly active in methane activation, leading to strong carbon deposition. Complementary reduction studies for  $\text{Sr}_2\text{CoMoO}_6$  indicated a similar instability in 5 %  $\text{H}_2/\text{Ar}$  mixtures, with the formation of  $\text{Sr}_3\text{MoO}_6$  and Co metal at and above 900 °C [43–49]. Also, in pure  $\text{CO}_2$ , partial decomposition into  $\text{SrCO}_3$ ,  $\text{SrMoO}_4$  and CoO was reported [45].

In our experiments, we generally observe a very high stability in the double perovskite structure, invariant of the gas atmosphere. Table 3 summarizes the phases, weight fractions, and changes in lattice parameters derived from the Rietveld refinement of the PXRD patterns shown in Figs. 2 and 3 for selected treatments. As a general introductory remark, we note that after either reduction treatment in  $\text{H}_2$  or  $\text{CO}_2/\text{CH}_4$ , a still intact Ni or Co (CoO)-mixed oxide-double perovskite interface partially prevails at varying extents.

With respect to the stability of  $\text{Sr}_2\text{NiMoO}_6$ , treatments in 1 bar flowing hydrogen at 800 °C (Fig. 2, Panel A) indicate a high stability of





**Fig. 3.** PXRD patterns collected on A-site deficient and Ni-doped  $\text{Sr}_2\text{CoMoO}_6$  samples. *Left column*, two top-most panels: A-site deficient  $\text{Sr}_{1.9}\text{CoMoO}_6$  before and after hydrogen treatment at  $800^\circ\text{C}$  followed by a DRM treatment up to  $800^\circ\text{C}$ . Two bottom-most panels: Ni–Co co-doped  $\text{Sr}_2\text{Co}_{0.9}\text{Ni}_{0.1}\text{MoO}_6$  before and after hydrogen treatment at  $800^\circ\text{C}$  followed by a DRM treatment up to  $800^\circ\text{C}$ . *Right column*: Ni–Co co-doped  $\text{Sr}_2\text{Co}_{0.5}\text{Ni}_{0.5}\text{MoO}_6$  before and after hydrogen treatment at  $800^\circ\text{C}$  followed by a DRM treatment up to  $800^\circ\text{C}$  and after one or two DRM treatments up to  $800^\circ\text{C}$  without hydrogen pre-reduction. Parameters: Hydrogen or DRM atmosphere ( $\text{CO}_2:\text{CH}_4:\text{He} = 1:1:1$ ), flow rate:  $60\text{ mL min}^{-1}$ , heating rate:  $5^\circ\text{C min}^{-1}$ .

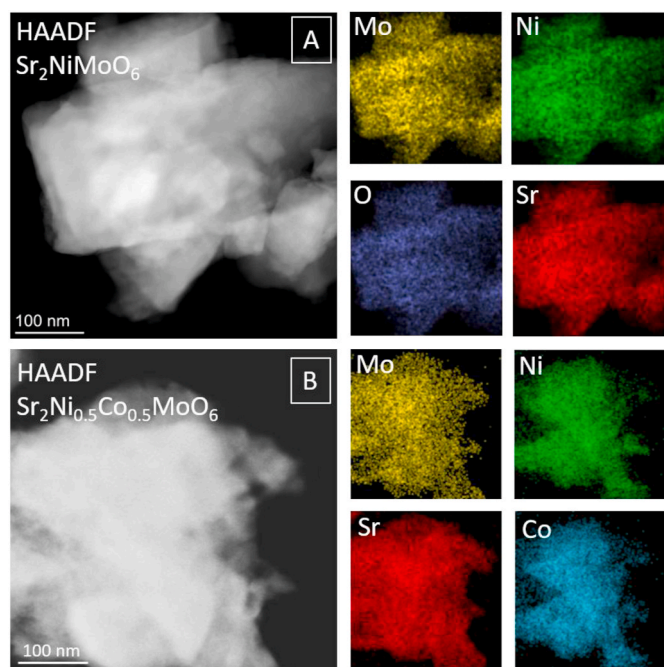
**Table 2**

Structure and unit-cell parameters of the different double perovskites after 48 h of sintering.

Sample	Structure [Space group]	Weight Fraction [wt.-%]	Cell parameters a [Å]	c [Å]
$\text{Sr}_2\text{NiMoO}_6$	$\text{Sr}_2\text{NiMoO}_6$ [I4/m]	98.9	5.5479	7.8957
	$\text{SrMoO}_4$ [I4 <sub>1</sub> /a]	1.1	5.3955	12.0199
$\text{Sr}_2\text{CoMoO}_6$	$\text{Sr}_2\text{CoMoO}_6$ [I4/m]	97.4	5.5676	7.9533
	$\text{SrMoO}_4$ [I4 <sub>1</sub> /a]	2.6	5.3955	12.0315
$\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$	$\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ [I4/m]	98.6	5.5549	7.9166
	$\text{SrMoO}_4$ [I4 <sub>1</sub> /a]	1.4	5.3905	12.0353

the double perovskite with only a minor amount of exsolved Ni particles (10.3 wt.-%). In the ex situ collected PXRD patterns after the hydrogen reduction, two features are worth noting, which will be in turn corroborated by the in situ measurements: first, the parasitic  $\text{SrMoO}_4$  structure, present after calcination, has vanished, and second,  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  appears as an additional phase. Striking is the fact that the latter exhibits a remarkably small crystallite size.  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is reported by Miranda et al. to be a strongly oxygen-deficient cubic double perovskite phase, whose thermodynamic stability strongly depends on the synthesis temperature [36]. Samples synthesized at temperatures lower than  $1400^\circ\text{C}$  inevitably transform to  $\text{SrMoO}_4$  upon annealing

[36]. We corroborate this finding, as the presence of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  (in mind that the temperature did not exceed  $800^\circ\text{C}$ ) is extremely sensitive to the reduction potential of the gas atmosphere. Whenever  $\text{Sr}_2\text{NiMoO}_6$  is exposed to a DRM mixture without hydrogen pre-reduction or a DRM treatment is performed after a hydrogen pre-reduction, the formation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is either suppressed or  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is removed by formation of additional  $\text{SrMoO}_4$ . The process of this transformation is further discussed in the context of the in situ PXRD experiments. However, to the best of our knowledge, we report it for the first time as a decomposition product of any strontium molybdate phase during reduction or catalytic treatments. After one and two DRM cycles, respectively, we observe that direct decomposition in a DRM mixture without prior pre-reduction yields a much higher amount of  $\text{SrMoO}_4$  compared to the calcined state and that the mixture composition hardly changes between the first and the second DRM cycle. The highest amount of  $\text{SrMoO}_4$  is observed after a hydrogen pre-reduction – DRM cycle. We will show in the in situ PXRD section that this is essentially due to the  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  –  $\text{SrMoO}_4$  intertransformation. Formation of Ni particles by exsolution in the DRM mixture has also been observed, although suppressed compared to after hydrogen reduction (3 wt.-% vs. 10 wt.-%).  $\text{SrCO}_3$  is also observed in small amounts (ca. 10 wt.-%), which is common for decomposed Sr-containing perovskites in DRM. Finally, the decomposition of  $\text{Sr}_2\text{NiMoO}_6$  is most pronounced by a pre-reduction step in hydrogen before a DRM experiment. Consequently, the amounts of  $\text{SrMoO}_4$ ,  $\text{SrCO}_3$  and exsolved Ni particles are highest in comparison to all other treatments.



**Fig. 4.** HAADF images and set of individual EDX maps (Mo–K, Ni–K, Co–K, O–K and Sr–K edges) for the  $\text{Sr}_2\text{NiMoO}_6$  (Panel A) and the  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  sample (Panel B).

This feature is corroborated by both TEM measurements and the catalytic experiments discussed in the subsequent sections.

The qualitative trends upon treating  $\text{Sr}_2\text{CoMoO}_6$  in hydrogen and during DRM in terms of phase formation are comparable to  $\text{Sr}_2\text{NiMoO}_6$ . One notable exception, which is at the core of the interpretation of the catalytic results in section 3.3., is that although metallic Co is detected after the hydrogen pre-reduction, DRM treatments either directly or after a pre-reduction without exception lead to the formation of CoO. This is again confirmed by TEM, the suppressed catalytic DRM activity (cf. section 3.3.) and also the XP spectra discussed below.

In accordance with the interpretation of the catalytic results based on the eventual activation of  $\text{Sr}_2\text{CoMoO}_6$  catalysts, the  $\text{Sr}_{1.9}\text{CoMoO}_6$ ,  $\text{Sr}_2\text{Co}_{0.9}\text{Ni}_{0.1}\text{MoO}_6$ , and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  materials were subjected to similar treatments (Fig. 3). In general, the structural behavior after hydrogen reduction and DRM treatments is very much comparable to pure  $\text{Sr}_2\text{CoMoO}_6$  or  $\text{Sr}_2\text{NiMoO}_6$ . Two notable exceptions are connected to the  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  phase: the latter appears already in the calcined state of  $\text{Sr}_2\text{Co}_{0.9}\text{Ni}_{0.1}\text{MoO}_6$ , but not in that of  $\text{Sr}_{1.9}\text{CoMoO}_6$ . As the formation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  depends on the availability of additional  $\text{Sr}^{2+}$  cations (formally, the base structure of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is close to  $\text{Sr}_3\text{Mo}^{6+}\text{O}_6$ , i.e., referenced to the starting structure  $\text{Sr}_2\text{M}^{2+}\text{MoO}_6$  either  $\text{Co}^{2+}$  or  $\text{Ni}^{2+}$  are formally replaced by  $\text{Sr}^{2+}$  as the structure does not contain either  $\text{Co}^{2+}$  or  $\text{Ni}^{2+}$ ) we must assume that Sr vacancies at the A-site are rather adverse to the formation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  (as they impede Sr substitution of Ni and/or Co). The most significant feature, however, is the extremely high amount of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  found in the hydrogen-reduced  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  sample (~50 wt.-%). Accompanied by this high amount of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is a splitting of the main peak of  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  into two peaks, which can be associated with isolated  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  and a single  $\text{SrMoO}_3$  perovskite structure. The latter compound represents a single perovskite phase that forms in case all Ni and Co, together with 1 mol SrO and oxygen is released reductively from  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ . We might also anticipate that the released SrO component is partially used under reductive conditions for  $\text{Co}^{2+}$  or  $\text{Ni}^{2+}$  substitution by  $\text{Sr}^{2+}$  toward  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$ . The reason why  $\text{SrMoO}_3$  is observed only for  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  after hydrogen reduction is the higher instability of this perovskite phase at the given chemical composition and the resulting

much higher degree of decomposition, yielding a higher amount of exsolved metal particles.  $\text{Sr}_2\text{Co}_{0.9}\text{Ni}_{0.1}\text{MoO}_6$ , on the other hand, is chemical composition-wise much closer to the pure  $\text{Sr}_2\text{CoMoO}_6$  and accordingly much more stable. Performing a DRM after hydrogen reduction in due course removes  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  (as observed previously), but also leads to almost complete destruction of the remaining double perovskite structures. Only about 6 wt.-% still prevail. The rest is a large amount of  $\text{SrMoO}_4$  (arising from the transformation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$ ),  $\text{SrCO}_3$  and, exsolved Ni/Co particles.

A common denominator in reduction studies of Sr–Mo containing double perovskites is the product variety. Thermodynamics at low  $P_{\text{O}_2}$  dictates the formation of metallic Ni and Co and a mixture of  $\text{Sr}_3\text{MoO}_4$  and  $\text{SrMoO}_4$  [43]. The former undergoes further transformation to  $\text{SrMoO}_3$  and SrO. Above 1583 °C, the formation of the  $\text{Sr}_2\text{MoO}_4$  Ruddlesden Popper type phase is observed [43]. Accordingly, the formation of  $\text{SrMoO}_3$  as the most reduced Sr–Mo oxide, exclusively for the least stable  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  phase, appears to be a logical conclusion based on the results of our studies conducted under the specified experimental conditions. The presence of apparently different strontium molybdate phases in our studies compared to literature-reported ones is a consequence of the different experimental conditions. As various strontium molybdates coexist within the phase diagram as a function of temperature and oxygen partial pressure, it is necessary to exercise precise control of humidity levels, as well as heating and cooling rates, in order to obtain the targeted phases [43]. For  $\text{Sr}_2\text{CoMoO}_6$ , the situation is further complicated by the possibility of Co-oxide exsolution from the double perovskite structure at low temperatures and high oxygen partial pressures, shifting the decomposition temperature of  $\text{Sr}_2\text{CoMoO}_6$  to higher temperatures [43]. This is essentially corroborated by our results.

The exsolution of Ni and Co from the respective perovskite structures has also been followed by electron microscopy (Fig. 5). After hydrogen reduction,  $\text{Sr}_2\text{NiMoO}_6$  shows clear signs of Ni exsolution (Panel A), with homogeneously distributed Ni particles between 10 and 50 nm. Similarly, exsolved Ni particles are also observed when  $\text{Sr}_2\text{NiMoO}_6$  is treated in the DRM mixture directly. Ni particle sizes are comparable, but the distribution is more heterogeneous. Co exsolution from  $\text{Sr}_2\text{CoMoO}_6$  (Panel C) after reduction in hydrogen is equally pronounced, but the morphology of exsolved Co appears more spatially extended and less particular. Extended, sometimes interconnected patches decorating the perovskite grain rims, are frequently observed. For the Ni and Co codoped double perovskite  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  we observe the exsolution of well-defined Ni–Co alloy particles in approximate sizes between 30 nm and 50 nm both if a hydrogen reduction at 800 °C is carried out prior to DRM (Panel D) or a DRM reaction is performed without hydrogen pre-reduction (Panel E). Most importantly, isolated Ni and/or Co particles are clearly underrepresented and almost exclusively, exsolved Ni–Co alloy particles have been observed in varying compositions. We have carried out on-particle EDX composition analysis for an array of particles of the  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  sample after hydrogen reduction/subsequent DRM and DRM without pre-reduction and we have highlighted five of them in Panels D and E. For particles 1 and 2 in Panel D, the compositions are approximately  $\text{NiCo}_{1.95}$  and  $\text{NiCo}_{1.63}$ , for the three particles in Panel E  $\text{NiCo}_{1.5}$ ,  $\text{NiCo}_{1.78}$  and  $\text{NiCo}_{1.1}$ . A statistical analysis reveals that in almost all cases, Co-richer Ni–Co alloy particles are exsolved. Furthermore, the deviation from the nominal and overall perovskite stoichiometry with respect to the Ni/Co ratio is significantly in favor of Co. The formation of Co-richer Ni–Co intermetallic nanoparticles upon exsolution is expected, as previous studies on the oxygen evolution reaction and transient oxidation of Ni–Co alloys have shown that the relative differences in the mobilities of  $\text{Ni}^{2+}$  and  $\text{Co}^{2+}$  ions lead to especially Co-richer surface regions with significant deviations from the nominal composition. This is corroborated both for the bulk and the surface by PXRD and XPS, respectively [44,45].

In conclusion, the principal findings of the PXRD and TEM experiments can be summarized as follows.

**Table 3**

Summary of the Rietveld-derived phases, weight fractions and lattice parameters for all samples after selected treatments.

Sample/Treatment	Phases	Weight Fraction [wt.-%]	a [Å]	b [Å]	c [Å]
Sr <sub>2</sub> NiMoO <sub>6</sub> calcined	Sr <sub>2</sub> NiMoO <sub>6</sub>	98.9	5.5479	–	7.8957
	SrMoO <sub>4</sub>	1.1	5.3955	–	12.0199
Sr <sub>2</sub> NiMoO <sub>6</sub> DRM	Sr <sub>2</sub> NiMoO <sub>6</sub>	69.7	5.5495	–	7.8976
	SrMoO <sub>4</sub>	13.7	5.3921	–	12.0532
	SrCO <sub>3</sub>	13.6	5.1051	8.3918	6.0552
	Ni	3.0	3.5239	–	–
	Sr <sub>2</sub> NiMoO <sub>6</sub>	71.2	5.5494	–	7.8953
Sr <sub>2</sub> NiMoO <sub>6</sub> DRM second cycle	SrMoO <sub>4</sub>	14.6	5.3938	–	12.0556
	SrCO <sub>3</sub>	10.9	5.1064	8.4014	6.0516
	Ni	3.3	3.5254	–	–
	Sr <sub>2</sub> NiMoO <sub>6</sub>	67.6	5.5487	–	7.8945
Sr <sub>2</sub> NiMoO <sub>6</sub> H <sub>2</sub> treatment	Sr <sub>11</sub> Mo <sub>4</sub> O <sub>23</sub>	22.1	16.3754	16.4369	16.4152
	Ni	10.3	3.5637	–	–
	Sr <sub>2</sub> NiMoO <sub>6</sub>	34.0	5.5507	–	7.8971
Sr <sub>2</sub> NiMoO <sub>6</sub> H <sub>2</sub> treatment & DRM	SrMoO <sub>4</sub>	35.1	5.3921	–	12.0583
	SrCO <sub>3</sub>	20.4	5.0979	8.4124	6.0477
	Ni	10.5	3.5246	–	–
	Sr <sub>2</sub> CoMoO <sub>6</sub>	97.4	5.5676	–	7.9533
Sr <sub>2</sub> CoMoO <sub>6</sub> calcined	SrMoO <sub>4</sub>	2.6	5.3955	–	12.0315
	Sr <sub>2</sub> CoMoO <sub>6</sub>	73.5	5.5689	–	7.9506
Sr <sub>2</sub> CoMoO <sub>6</sub> DRM	SrMoO <sub>4</sub>	13.6	5.3940	–	12.0400
	SrCO <sub>3</sub>	10.3	5.1025	8.4081	6.0398
	CoO	2.7	4.2677	–	–
	Sr <sub>2</sub> CoMoO <sub>6</sub>	74.9	5.5724	–	7.9441
	Sr <sub>11</sub> Mo <sub>4</sub> O <sub>23</sub>	16.8	16.5118	16.4345	16.3424
Sr <sub>2</sub> CoMoO <sub>6</sub> H <sub>2</sub> treatment	Co	8.3	3.5464	–	–
	Sr <sub>2</sub> CoMoO <sub>6</sub>	44.0	5.5751	–	7.9458
	SrMoO <sub>4</sub>	30.4	5.3903	–	12.0556
Sr <sub>2</sub> CoMoO <sub>6</sub> H <sub>2</sub> treatment & DRM	SrCO <sub>3</sub>	22.7	5.1050	8.4168	6.0429
	CoO	2.9	4.2543	–	–
	Sr <sub>1.9</sub> CoMoO <sub>6</sub>	23.7	5.5747	–	7.9385
	SrMoO <sub>4</sub>	43.2	5.3932	–	12.0515
Sr <sub>2</sub> Co <sub>0.9</sub> Ni <sub>0.1</sub> MoO <sub>6</sub> H <sub>2</sub> treatment & DRM	SrCO <sub>3</sub>	28.7	5.1039	8.4143	6.0437
	CoO	4.3	4.2615	–	–
	Sr <sub>2</sub> Co <sub>0.9</sub> Ni <sub>0.1</sub> MoO <sub>6</sub>	26.2	5.5758	–	7.9470
	SrMoO <sub>4</sub>	37.4	5.3905	–	12.0507
	SrCO <sub>3</sub>	26.3	5.1032	8.4073	6.0398
Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub> calcined	Co	10.1	3.5445	–	–
	Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub>	98.6	5.5549	–	7.9166
	SrMoO <sub>4</sub>	1.4	5.3905	–	12.0353
Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub> DRM	Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub>	60.7	5.5405	–	7.8826
	SrMoO <sub>4</sub>	20.7	5.3700	–	11.9958
	SrCO <sub>3</sub>	15.1	5.0738	8.3638	5.9942
	Ni/Co	3.6	3.2224	–	–
	Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub>	38.7	5.5460	–	7.8950
Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub> DRM second cycle	SrMoO <sub>4</sub>	26.6	5.3771	–	12.0073
	SrCO <sub>3</sub>	24.0	5.0904	8.3846	6.0205
	Ni/Co	10.7	3.5208	–	–
	Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub>	19.0	5.6103	–	8.0002
Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub> H <sub>2</sub> treatment	SrMoO <sub>3</sub>	17.4	5.5608	–	7.9181
	Sr <sub>11</sub> Mo <sub>4</sub> O <sub>23</sub>	51.2	16.4250	16.4654	16.4025
	Ni/Co	12.4	3.5538	–	–
	Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub>	6.3	5.5643	–	7.9336
Sr <sub>2</sub> Ni <sub>0.5</sub> Co <sub>0.5</sub> MoO <sub>6</sub> H <sub>2</sub> treatment & DRM	SrMoO <sub>4</sub>	40.1	5.3892	–	12.0552
	SrCO <sub>3</sub>	39.2	5.1053	8.4112	6.0368
	Ni/Co	14.4	3.5378	–	–

- SrMoO<sub>4</sub> is formed, whenever either of the samples is annealed in the dry reforming mixture and its formation during DRM is accelerated, if a hydrogen pre-reduction is carried out.
- SrMoO<sub>4</sub> is always absent, if only a hydrogen pre-reduction is carried out.
- Sr<sub>11</sub>Mo<sub>4</sub>O<sub>23</sub> is formed by hydrogen reduction only and its appearance is a direct consequence of the cation-defective nature of the perovskite in reductive atmospheres due to the exsolution of Co/Ni. In less-reducing environments, such as DRM mixtures, Sr<sub>11</sub>Mo<sub>4</sub>O<sub>23</sub> is rapidly transformed to SrMoO<sub>4</sub>.
- The formation of SrMoO<sub>3</sub> is a direct consequence of a more pronounced reductive decomposition propensity of a rather unstable double perovskite phase. A prerequisite for the formation is the rapid

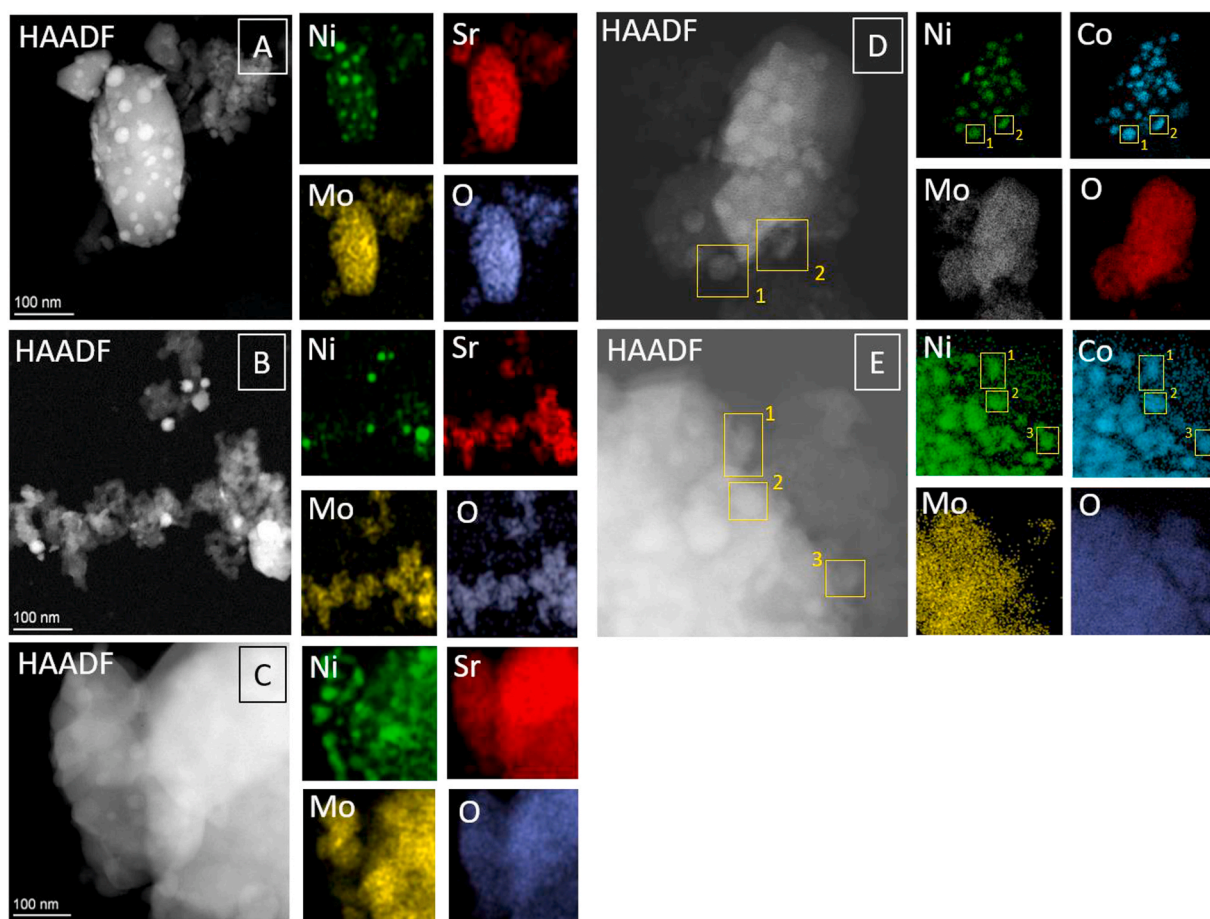
leaching of the B-site ions as exsolved metal particles from the perovskite structure, accompanied by the loss of SrO.

- Ni- and Co-co-doped strontium molybdate double perovskites tend to exsolve slightly Co-enriched NiCo alloy particles, but not isolated Ni and Co nanoparticles.

Phase and structure evolution during hydrogen reduction and DRM operation monitored by in situ X-ray diffraction analysis.

As we have shown in recent studies for doped single perovskites, a clear understanding of the correlation between structure and activity is only possible by in situ monitoring those changes during hydrogen reduction and DRM operation [5,8,9,50,51]. Fig. 6 shows the in situ collected PXRD patterns during a hydrogen pre-reduction treatment, followed by a DRM cycle between 25 °C and 800 °C, and Fig. 7 shows the



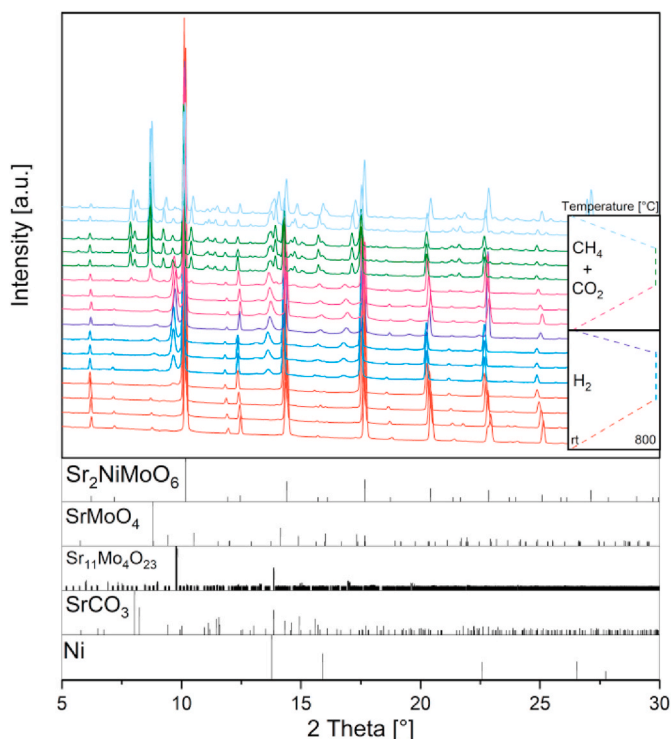


**Fig. 5.** HAADF-STEM and EDX analysis of  $\text{Sr}_2\text{NiMoO}_6$  after reduction in hydrogen at  $800^\circ\text{C}$ , followed by a DRM treatment up to  $800^\circ\text{C}$  (Panel A), after a DRM treatment up to  $800^\circ\text{C}$  without hydrogen pre-reduction (B),  $\text{Sr}_2\text{CoMoO}_6$  after hydrogen reduction at  $800^\circ\text{C}$  (Panel C),  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  after a DRM treatment up to  $800^\circ\text{C}$  with hydrogen pre-reduction (Panel D) and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  after a DRM treatment up to  $800^\circ\text{C}$  without hydrogen pre-reduction (Panel E).

associated weight fraction analysis based on Rietveld refinement. We show the waterfall plot of the diffractograms only for  $\text{Sr}_2\text{NiMoO}_6$ , but provide for other representative samples only the weight fraction analysis (Fig. 7). The respective diffractograms are presented in summary form in the Supporting Information (Figs. S1–S3). During heating in hydrogen up to  $775^\circ\text{C}$ , the double perovskite structure is remarkably stable and only above this temperature, and during the isothermal phase, the formation of the  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  structure takes place and becomes strongly accelerated during the holding period at  $800^\circ\text{C}$ . In parallel, we observe the beginning exsolution of Ni. Switching to a DRM mixture after re-cooling causes the formation of  $\text{SrMoO}_4$  and  $\text{SrCO}_3$  at the expense of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  at  $500^\circ\text{C}$ . The weight fraction of Ni is essentially constant during the DRM heating up to  $800^\circ\text{C}$  and also during the isothermal period at  $800^\circ\text{C}$ . Decomposition of  $\text{Sr}_2\text{NiMoO}_6$  and an associated further increase of  $\text{SrMoO}_4$  and  $\text{SrCO}_3$  is observed above  $725^\circ\text{C}$  and during the isothermal phase of the experiment. Upon reaching the isothermal phase, the composition of the mixture reaches a steady state, which is also observed during re-cooling. If no hydrogen pre-reduction is carried out prior to DRM, hardly any changes are observed during the first DRM cycle up to  $800^\circ\text{C}$  Ni exsolution, as well as formation of  $\text{SrMoO}_4$  and  $\text{SrCO}_3$  are only observed during the 10 min isothermal period at  $800^\circ\text{C}$ . During the second DRM cycle, the multi-phase mixture containing  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{SrMoO}_4$ , Ni and  $\text{SrCO}_3$  has evidently essentially reached a steady state. A slight increase in  $\text{SrMoO}_4$  is observed, but again, most of the change in the composition of the sample is only observed during the isothermal period at  $800^\circ\text{C}$ . If similar experiments are carried out on the Ni- and Co-co-doped material, we note a similar stability of the  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  structure up to  $800^\circ\text{C}$ .

$^\circ\text{C}$ . Some Ni exsolution is observed beginning at around  $670^\circ\text{C}$  alongside the formation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$ , which takes place between  $670^\circ\text{C}$  and  $800^\circ\text{C}$ . After 10 min at  $800^\circ\text{C}$ , some decomposition of  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  is observed (to around 90 wt.-%). A DRM treatment after the hydrogen reduction does not affect the  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  very much, but rather the re-transformation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  into  $\text{SrMoO}_4$ , accompanied by the formation of  $\text{SrCO}_3$  and Ni exsolution. Surprisingly,  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  appears to be less stable in a DRM mixture without hydrogen pre-reduction. Here, the partial decomposition of  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  starts at around  $750^\circ\text{C}$ , concurrently with the formation of additional  $\text{SrMoO}_4$ . After a 10 min isothermal period at  $800^\circ\text{C}$ , the ratio of  $\text{SrMoO}_4$ , NiCo alloy and  $\text{SrCO}_3$  is somewhat comparable to the state shown in Panel F after the DRM reaction, although the amount of  $\text{SrMoO}_4$  appears a little bit more pronounced, as is the amount of decomposed  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ . It should be noted that all the Co-based  $\text{Sr}_2\text{CoMoO}_6$  samples for the ex situ benchmark treatments in hydrogen were heated to  $900^\circ\text{C}$  for the ex situ benchmark treatments in hydrogen induce the decomposition of  $\text{Sr}_2\text{CoMoO}_6$ . Hence, the pronounced formation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  during hydrogen pre-reduction discussed in the context of Fig. 3 cannot be seen in the in situ experiments, as the maximum temperature was  $800^\circ\text{C}$ . Nevertheless, we propose a lower threshold of  $800^\circ\text{C}$  for the structural transformations under discussion. Again, the in situ PXRD data suggest that  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  is a transient Sr-enriched Ni/Co cation-deficient phase, which is only reductively formed in the absence of  $\text{CO}_2$  and subsequently decomposes upon SrO removal during DRM in the presence of  $\text{CO}_2$ .





**Fig. 6.** In situ PXRD analysis of  $\text{Sr}_2\text{NiMoO}_6$  for a hydrogen reduction (up to 800 °C) – DRM cycle (up to 800 °C). Hydrogen flow: 1 mL min<sup>-1</sup> from 25 °C to 800 °C; DRM flow consisting of  $\text{CO}_2:\text{CH}_4 = 1:1$ , 1 mL min<sup>-1</sup> from 25 °C to 800 °C. The heating program is shown as inset.

### 3.2.2. Surface chemical aspects of hydrogen treatment and DRM operation

Complementary to bulk analysis, we studied the surface chemical composition by X-ray photoelectron spectroscopy for  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{CoMoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  in the calcined state, after hydrogen reduction at 800 °C ( $\text{Sr}_2\text{NiMoO}_6$ ) and 900 °C ( $\text{Sr}_2\text{CoMoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ ) and after direct DRM treatment up to 800 °C. The spectra are shown in Figs. 8 and 9, Tables S1 and S2 in the Supporting Information summarize the peak positions of the fitted components, their FWHM and raw area, as well as the atomic percentages. For  $\text{Sr}_2\text{NiMoO}_6$ , the untreated sample after calcination reveals the typical features for NiO, with the Ni 2p<sub>3/2</sub> and Ni 2p<sub>1/2</sub> peaks at 856.0 eV and 873.9 eV, alongside the two satellite peaks at 861.7 eV and 879.8 eV (topmost spectrum in Panel A) [52–56]. After the reduction in hydrogen, a second doublet feature with pronounced asymmetry, including the associated satellite peaks, typical for metallic Ni, appears at 852 eV and 869.7 eV. The respective satellites are found at 858.0 eV and 875.4 eV, respectively (middle spectrum in Panel A). After a direct DRM treatment, the same set of peaks is obtained, however, the contribution of the metallic Ni component is smaller compared to after hydrogen treatment. This is in clear agreement with the less reducing environment in DRM mixture. Overall, the Ni 2p spectra in the calcined state agree well with literature-reported spectra of  $\text{Sr}_2\text{NiMoO}_6$  [57]. While the Sr 3d and O 1s peaks do not yield solid interpretable features, clear changes can be found for the Mo 3d peaks as a function of treatment (Panel B). Even in the calcined state, contributions of Mo<sup>6+</sup> and Mo<sup>5+</sup> at positions of 233.0 eV and 236.2 eV (Mo<sup>6+</sup>), as well as 231.6 eV and 235.0 eV (Mo<sup>5+</sup>), are observed, which indicate the presence of oxygen vacancies for the charge compensation [58–63]. After hydrogen reduction, the contribution of Mo<sup>5+</sup> is diminished in favor of Mo<sup>4+</sup>, resulting from  $\text{Sr}_2\text{NiMoO}_6$  reduction. In principle, in line with the evolution of the Ni 2p peaks, no Mo<sup>4+</sup> contribution is observed after DRM treatment due to the less reducing environment. The strong increase in Mo<sup>5+</sup> after DRM

treatment results from the defect interactions, which the DRM mechanism on perovskite structures is known for, as e.g., described in Ref. [64]. In summary, the XPS results indicate a slightly reduced  $\text{Sr}_2\text{NiMoO}_6$  sample even after calcination with a certain amount of oxygen vacancies. The number of the latter is clearly increased both by hydrogen reduction or DRM treatment.

$\text{Sr}_2\text{CoMoO}_6$  exhibits the same evolution under hydrogen reduction and DRM treatment. For  $\text{Sr}_2\text{CoMoO}_6$ , the Co 2p spectrum in the calcined state represents the typical spectrum for Co<sup>2+</sup> (peaks at 779.7 eV and 795.4 eV for Co 2p<sub>3/2</sub> and Co 2p<sub>1/2</sub>, satellite peaks at 785.1 eV and 801.2 eV, Co LMM Auger transition at 772.1 eV) and is more indicative of CoO, than Co<sub>3</sub>O<sub>4</sub> (topmost spectrum in Panel C) [65–69]. As for Ni 2p, Co metal is also found in surface-near regions, both after hydrogen reduction and DRM treatment, respectively. Again, the contribution of Co metal is less pronounced after a direct DRM treatment. The Mo 3d peaks follow a similar trend as those observed for  $\text{Sr}_2\text{NiMoO}_6$ , with two pronounced differences: derived from the much more pronounced Mo<sup>5+</sup> intensity already after calcination, we infer a higher number of oxygen vacancies for  $\text{Sr}_2\text{CoMoO}_6$ , which after DRM give rise to a significant Mo<sup>4+</sup> contribution not observed for  $\text{Sr}_2\text{NiMoO}_6$ .

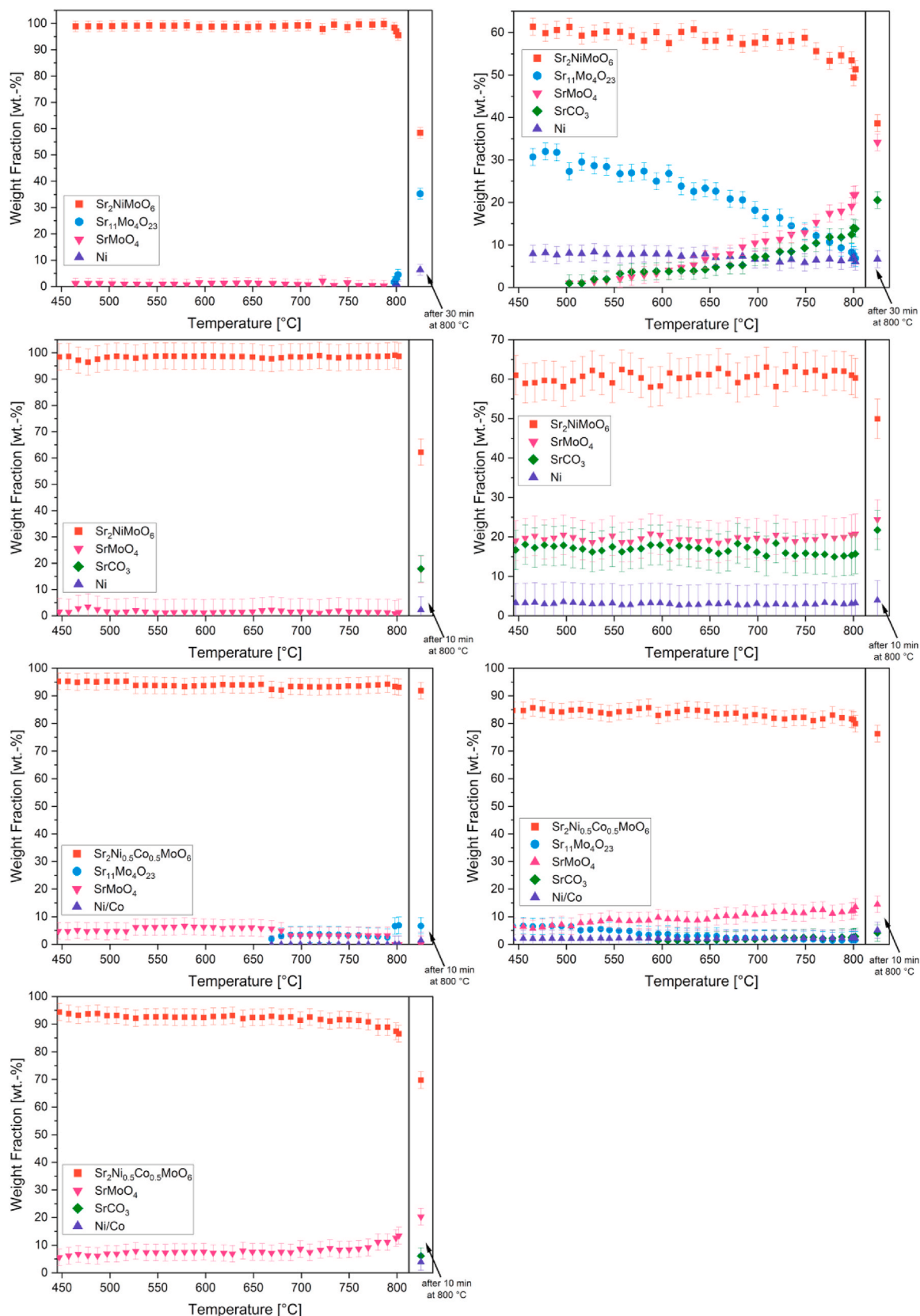
Most important for the interpretation of the catalytic results in the subsequent chapter, the corresponding spectra for  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  reveal a substantial difference in the Co 2p region: while the metallic Co component for  $\text{Sr}_2\text{CoMoO}_6$  after a DRM treatment is clearly underrepresented in comparison to the oxidic component (roughly 1:10 = Co metal:Co oxidic as determined from the area ratios of the Co 2p<sub>3/2</sub> peaks), this ratio changes to 1.5:1 = Co metal:Co oxidic for  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ . This indicates that co-alloying with Ni leads to a higher amount of metallic Co in the surface near regions, through the exsolution of Co-rich Ni–Co alloy nanoparticles, as evidenced by TEM (cf. Fig. 4). This presence of metallic Ni–Co states is paramount for the activation of  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  during DRM (cf. Fig. 10). The Mo 3d peaks follow the same trend as  $\text{Sr}_2\text{NiMoO}_6$  with the distinct difference that after calcination, co-doping the perovskite with Ni and Co leads to more reduced Mo species. We address this to a higher amount of oxygen vacancies. During exsolution the depletion of B-site atoms leads to the oxidation of Mo species to level again with  $\text{Sr}_2\text{NiMoO}_6$ .

### 3.2.3. Carbon resilience

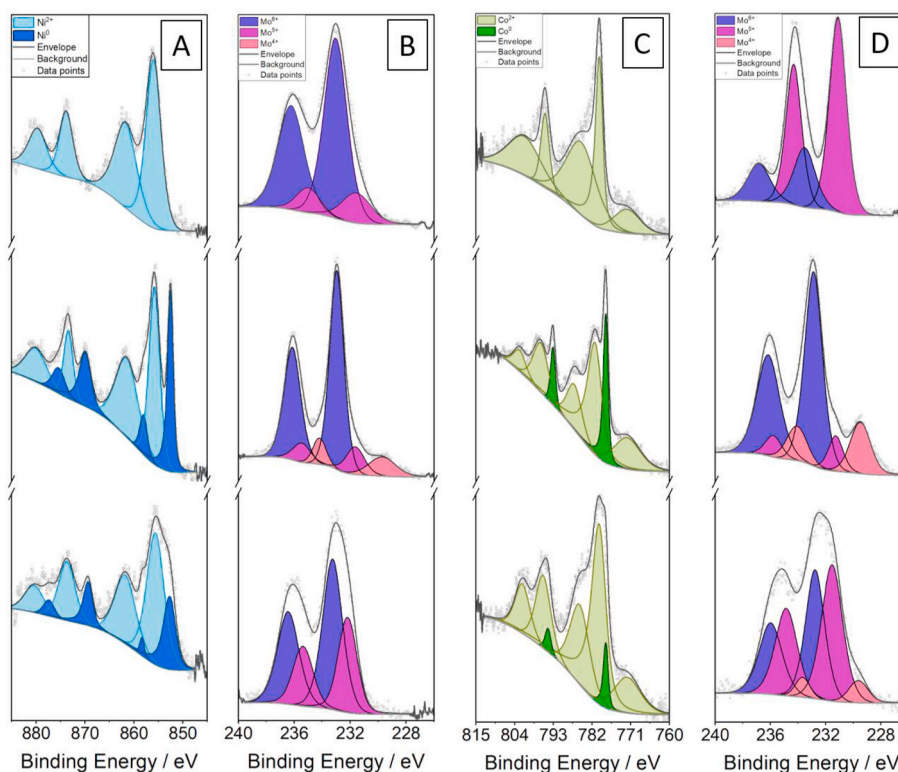
We also briefly addressed the potential coking issue of all materials during DRM operation in comparison to the calcined and the hydrogen-prereduced state. Fig. S4 shows a representative set of C 1s spectra collected on  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ , which indicate no carbon in the calcined state (bottom spectrum) and roughly comparable, but minute amounts after hydrogen and DRM treatment (middle and top spectrum, respectively), as judged by the intensity of the graphitic carbon component at 284.6 eV. We tentatively address this suppressed coke formation by the catalytic experiments highlighted in Fig. 10: due to the high reverse water-gas shift activity and the still remaining carbon dioxide in the product mixture, the reaction-formed water is able to efficiently burn off carbon from the catalyst surface. The observed carbon signals are, thus, rather a consequence of the contact to ambient conditions after the treatments. In summary, under the chosen experimental conditions – also in line with the catalytic profiles discussed below – none of the catalysts shows significant carbon deposition or coking effects in neither electron microscopy nor XPS, despite the rather large Ni, Co or Ni–Co particles.

### 3.3. Catalytic methane dry reforming performance

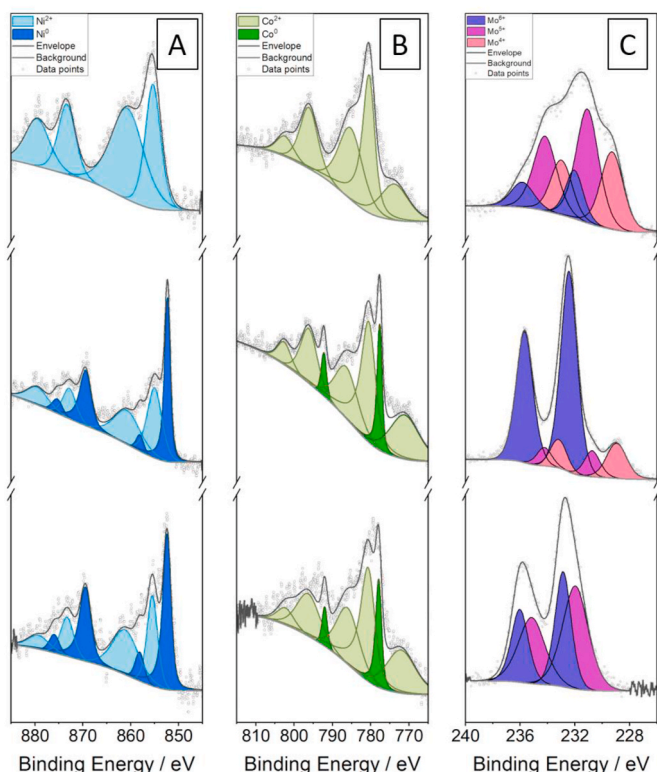
Fig. 10 shows the catalytic methane dry reforming performance in a comparative fashion for  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{CoMoO}_6$  and  $\text{Sr}_2\text{Ni}_x\text{Co}_{1-x}\text{MoO}_6$ . We have performed all measurements with and without a hydrogen pretreatment to trigger eventual metal exsolution and formation of a metal-perovskite heterointerface and to assess the catalytic differences upon direct treatment in a DRM mixture and DRM after a preceding



**Fig. 7.** Weight fraction analysis based on the Rietveld refinements of the in situ PXRD data for  $\text{Sr}_2\text{NiMoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  after different pre-reduction and DRM treatments. *Top row, left panel:*  $\text{Sr}_2\text{NiMoO}_6$  during pre-reduction in hydrogen up to 800 °C; *Top row, right panel:*  $\text{Sr}_2\text{NiMoO}_6$  during DRM up to 800 °C after the pre-reduction treatment is shown in the left panel. *Second-most row from the top:*  $\text{Sr}_2\text{NiMoO}_6$  during the first (Left Panel) and the second DRM cycle without hydrogen pre-reduction (Right panel). *Second-most row from the bottom:*  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  during pre-reduction in hydrogen up to 800 °C (Left Panel),  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  during DRM up to 800 °C after the pre-reduction treatment shown in the right panel. *Bottom row:*  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  during a first DRM cycle without hydrogen pre-reduction. Parameters: DRM atmosphere  $\text{CO}_2:\text{CH}_4 = 1:1$ , flow rate: 40 mL min<sup>-1</sup>, heating rate: 5 °C min<sup>-1</sup>.



**Fig. 8.** Ni 2p, Co 2p<sub>3/2</sub> and Mo 3d high-resolution XP spectra in the calcined, hydrogen-reduced and post-DRM state (from top to bottom) for Sr<sub>2</sub>NiMoO<sub>6</sub> and Sr<sub>2</sub>CoMoO<sub>6</sub>. Panel A: Ni 2p Sr<sub>2</sub>NiMoO<sub>6</sub>; Panel B: Mo 3d Sr<sub>2</sub>NiMoO<sub>6</sub>; Panel C: Co 2p Sr<sub>2</sub>CoMoO<sub>6</sub>. Panel D: Mo 3d Sr<sub>2</sub>CoMoO<sub>6</sub>.

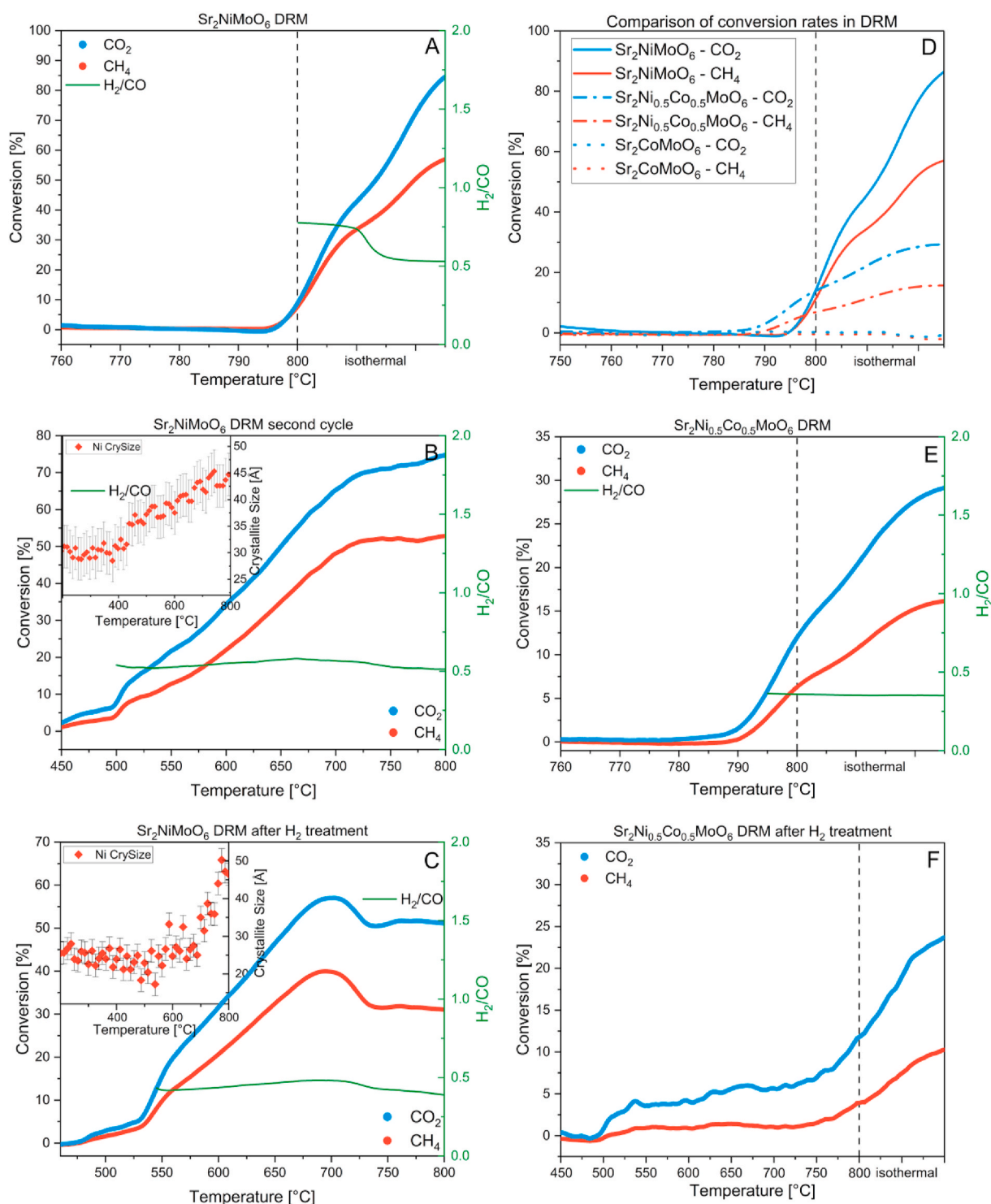


**Fig. 9.** Ni 2p, Co 2p<sub>3/2</sub> and Mo 3d high-resolution XP spectra in the calcined, hydrogen-reduced and post-DRM state (from top to bottom) for Sr<sub>2</sub>Ni<sub>0.5</sub>Co<sub>0.5</sub>MoO<sub>6</sub>. Panel A: Ni 2p; Panel B: Co 2p; Panel C: Mo 3d.

hydrogen exposure.

Without hydrogen treatment, Sr<sub>2</sub>NiMoO<sub>6</sub> reveals a steep acceleration of activity at around 795 °C during the first DRM cycle (Panel A). In the beginning, and roughly in the first minute of the isothermal section at 800 °C, the carbon dioxide and methane conversion match. After that, the carbon dioxide conversion is significantly enhanced and reaches conversion levels of ca. 85 %, while methane conversion reaches only about 55 %. The reason for this obvious deviation from stoichiometric DRM conversion is the pronounced reverse-water gas shift activity observed for Sr<sub>2</sub>NiMoO<sub>6</sub>. This leads to the additional formation of carbon monoxide and water and is directly reflected in the H<sub>2</sub>/CO ratio. We observe a ratio of ~0.8 in the temperature region, where the carbon dioxide and methane traces match, indicating almost exclusive DRM activity. Above, this ratio drops to around 0.5 in line with increased reverse water gas shift activity. During the second DRM cycle, the onset of catalytic activity is markedly shifted to lower temperatures, i.e., to about 450 °C. Again, a slight deviation from stoichiometric DRM conversion of carbon dioxide and methane has been observed, saturating at conversion levels of 70 % and 50 % for carbon dioxide and methane, respectively (Panel B). If a hydrogen pre-treatment at 800 °C is carried out before the DRM test (Panel C), the onset temperature is comparable to that observed in the second DRM cycle without hydrogen pre-reduction, as are the conversion levels at 700 °C. However, a peak in the conversion is observed both for carbon dioxide and methane at around 700 °C. At higher temperatures, the conversion drops by about 10 % and subsequently approaches a constant lower level beyond 725 °C. The reason for this behavior is shown as an inset in Panel C: starting at around 650 °C, but accelerating strongly up to 800 °C, the Ni crystallite sizes more than double from 20 nm to 50 nm in the same temperature window. Hence, the decrease in catalytic conversion coincides with strong Ni crystallite sintering, which leads to an overall activity loss within the catalyst bed due to a decrease of available active Ni surface sites. This behavior is only observed for the hydrogen pre-treated sample and is somewhat also somewhat reflected in the TEM images and EDX





**Fig. 10.** Methane dry reforming performance of  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{CoMoO}_6$  and  $\text{Sr}_2\text{Ni}_x\text{Co}_{1-x}\text{MoO}_6$  after selected treatments as indicated in the individual panels. Parameters: DRM atmosphere  $60 \text{ mL min}^{-1}$  ( $\text{CH}_4:\text{CO}_2:\text{He} = 1:1:1 \text{ mL min}^{-1}$ ); catalyst mass: 200 mg; heating rate:  $5^\circ\text{C min}^{-1}$ . Blue traces: carbon dioxide conversion, red traces: methane conversion. Isothermal sections: 10 min each. The green profiles in Panels A, B, C and E highlight the respective  $\text{H}_2/\text{CO}$  ratios (axis on the right side).

maps shown in Fig. 5. Again, the  $\text{H}_2/\text{CO}$  ratio determined at  $\sim 0.5$  (Panel C, also valid for the profiles shown in Panels B and E) indicates strong contribution of the reverse water-gas shift reaction. Focussing on the DRM performance of  $\text{Sr}_2\text{CoMoO}_6$ , we at first recall that pronounced Co metal exsolution is indeed observed after hydrogen pre-treatment at  $800^\circ\text{C}$ , but hardly any is detectable after DRM up to  $800^\circ\text{C}$  (Fig. 8, Panel C, middle and bottom spectra). Due to the instability/absence of

$\text{Co}^0$  at the surface under DRM conditions, no catalytic activity is observed (Panel D). We have subsequently focussed on different activation strategies, including introducing defects at the A-site to facilitate decomposition of the perovskite (compare Fig. 3), but equally, no substantial enhancement in either Co exsolution or DRM activity was observed. In due course, we opted for Ni co-alloying, i.e., introducing different doping levels of Co with Ni to eventually increase the DRM



performance. Two different doping levels with nominal compositions  $\text{Sr}_2\text{Ni}_{0.1}\text{Co}_{0.9}\text{MoO}_6$  and  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  were prepared and tested. While the activity increase for the former is only minute, a pronounced activity increase was observed for the latter (Panel D, E and F). In short, the onset temperature and the behavior upon hydrogen pre-treatment and DRM performance with and without hydrogen pre-treatment are comparable to  $\text{Sr}_2\text{NiMoO}_6$ . The only pronounced difference is the overall lower maximum conversion (carbon dioxide 30 %, methane 15 % during the first DRM cycle), which can be interpreted in terms of a lower number and/or activity of mixed metallic surface sites relative to the activated  $\text{Sr}_2\text{NiMoO}_6$  material. We, thus, conclude that the addition of Ni suppresses the oxidation propensity of Co to some extent, causing the observed activity via stabilized metallic surface sites. This is directly reflected in the XP spectra discussed in Figs. 8 and 9. Note that EDX experiments also prove that indeed Ni–Co alloy particles are primarily exsolved, and no isolated Ni and/or Co particles. By comparing the catalytic performance to similar systems described in the literature, we note that the catalytic activity in terms of conversion and  $\text{H}_2/\text{CO}$  ratio is in line with previously reported systems, e.g. in Fe-doped  $\text{Sr}_2\text{NiMoO}_6$  materials. Carillo et al. reported exsolution of  $\text{FeNi}_3$  alloy nanoparticles following a pre-reduction treatment in hydrogen for prolonged times (2–20 h) at 900 °C, which also caused partial breakdown of the parent double perovskite structure. Carbon dioxide and methane conversion levels were observed at 70–80 % and 50 % for reaction temperatures of 850 °C, respectively, with  $\text{H}_2/\text{CO}$  ratios not exceeding 0.5 [17]. Also in line with our results, the authors claimed that the competing reverse water-gas shift reaction was responsible for this phenomenon. In terms of a comparative discussion between Ni- and Co-containing double perovskites, Hossain et al. provided such measurements for different  $\text{La}_2\text{Ni}(\text{Co})\text{MnO}_6$  samples. Very high carbon dioxide and methane conversion levels were observed at 800 °C reaction temperatures for 100 h time-on-stream on  $\text{La}_2\text{NiMnO}_6$ . Also, for these systems, the carbon dioxide conversion was higher than that for methane. The purely Ni-containing materials performed consistently better compared to the purely Co-doped ones in terms of conversion and a  $\text{H}_2/\text{CO}$  ratio value of close to unity.  $\text{La}_2\text{NiMnO}_6$  decomposes in the DRM mixture into  $\text{La}_2\text{O}_3$ ,  $\text{La}(\text{OH})_3$ ,  $\text{MnO}$ ,  $\text{NiO}$  and  $\text{Ni}$ . As for the studied  $\text{La}_2\text{NiCoO}_6$  material, which features  $\text{La}_2\text{O}_3$ ,  $\text{Ni}$ ,  $\text{NiO}$  and  $\text{CoO}$  in the aged catalyst after 10 h time-on-stream, we note that separate peaks for Ni,  $\text{NiO}$  and  $\text{CoO}$  are observed, i.e. it cannot be ruled out by that study, whether the activity in  $\text{La}_2\text{NiCoO}_6$ , in fact, arises from the present Ni-containing phases, which feature a much better DRM performance [70]. Similar deactivation effects of preferred Co oxidation in Co-rich Ni–Co particles are also observed on non-perovskite catalysts, i.e.,  $\text{Ce}_{0.75}\text{Zr}_{0.25}\text{O}_{2-\delta}$  decorated with 3 wt.-% Ni–Co particles [71]. Table S3 summarizes the conversion performance at comparable gas hourly space velocity (GHSV) values of  $\text{Sr}_2\text{NiMoO}_6$ ,  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$  in comparison to  $\text{LaNiO}_3$ ,  $\text{Ni}/\text{Al}_2\text{O}_3$  and selected literature-reported perovskite systems in DRM.  $\text{CO}_2$  conversion levels at comparable reaction temperatures are essentially similar to or better than other Ni- and Co-containing perovskites. Compared to  $\text{Ni}/\text{Al}_2\text{O}_3$  and  $\text{LaNiO}_3$ , the reverse water-gas shift activity of our materials is pronounced, and as such, is clearly dominated by the perovskite phases – as indicated by the consistently lower  $\text{CH}_4$  conversions. As mostly also observed in the literature, the Co-containing phases feature worse than their Ni counterparts. Differences in conversion levels and catalytic activity can be mostly related to different extents of perovskite structure decomposition and the associated exsolution of Ni and/or Co particles. In contrast to most studies in literature, our Mo-based perovskites are almost exclusively structurally very stable and in most cases, the perovskite structure is at least partially retained despite exsolution effects.

With respect to structure-activity correlations, i.e., the elucidation of the direct impact of any of the dynamically formed phases on DRM activity, we note that it affects essentially three different phases, except of exsolved Ni:  $\text{SrMoO}_4$ ,  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  and  $\text{SrCO}_3$ . If we correlate the in situ XRD data with the catalytic profiles, we note that during the DRM

experiment after the hydrogen pretreatment, the amount of  $\text{SrMoO}_4$  essentially remains constant between 400 °C and 800 °C, although the activity onset is observed at 450 °C with a strong acceleration at higher reaction temperatures. The strong resemblance of the DRM profile after hydrogen reduction and the second DRM profile without such pre-reduction in terms of DRM onset temperature and conversion levels, as well as the constant amount of  $\text{SrMoO}_4$  during the second DRM cycle, indicates that  $\text{SrMoO}_4$  is merely a spectator species. The same is true for  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$ . It disappears during DRM with no apparent impact on DRM activity, i.e., there is no correlation between the structural transformation of  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  into  $\text{SrMoO}_4$  and enhanced/diminished catalytic DRM activity.  $\text{SrCO}_3$  appears as a reaction product of Sr phases with  $\text{CO}_2$ , but also acts as a spectator species according to in situ XRD. We therefore suspect that none of these phases without Ni exhibit DRM activity. It appears that the DRM activity is essentially driven by the exsolved Ni, Co or Ni–Co particles in possible combination with oxygen vacancies of the remaining double perovskite structure.

#### 4. Conclusions

We have focused on a series of  $\text{Sr}_2\text{MMoO}_6$  ( $\text{M} = \text{Ni}, \text{Co}$  and  $(\text{Ni}, \text{Co})$ ) compounds as representative model systems to highlight the capabilities of double perovskites as eventual precursor materials for methane dry reforming (DRM) applications. The key findings can be summarized as follows.

- *Stability of the double perovskite structures:* Phase-wise, pre-treatments in either pure hydrogen or dry reforming  $\text{CO}_2/\text{CH}_4$  mixtures exclusively yield partial decomposition of the initial double perovskites through exsolution of Ni or CoO particles and the associated formation of parasitic phases, such as  $\text{SrMoO}_4$  or  $\text{SrCO}_3$  (in DRM mixtures).
- *Formation of the transient  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  phase:* The formation of an oxygen-deficient and Sr-rich  $\text{Sr}_{11}\text{Mo}_4\text{O}_{23}$  transient compound has been revealed by in situ powder X-ray diffraction measurements in pure hydrogen only, representing a key intermediate for double perovskite decomposition following DRM treatments.
- *Why Co-containing double perovskites are less active compared to their Ni-containing counterparts:* The main difference between the Ni- and Co-containing Sr molybdate perovskites (despite partial decomposition) is the much stronger oxidation propensity of exsolved Co, most likely by oxygen supply from the partially intact double perovskite structure and/or oxidation by the DRM gas phase. For  $\text{Sr}_2\text{NiMoO}_6$ , the resulting metallic Ni-double perovskite interface is DRM- and reverse water-gas shift active, both if a pre-reduction step in hydrogen is carried out before the DRM experiment or if  $\text{Sr}_2\text{NiMoO}_6$  is directly decomposed in the DRM mixture.
- *Activation of  $\text{Sr}_2\text{CoMoO}_6$ :* Different strategies to improve the catalytic activity, including hydrogen by-mixing, A-site deficiency or co-alloying with Ni have been followed, but only the latter has a beneficial effect at Ni-rich compositions close to a Co:Ni = 1:1 ratio on enhancing the DRM activity. In  $\text{Sr}_2\text{Ni}_{0.5}\text{Co}_{0.5}\text{MoO}_6$ , the substitution of Co by Ni suppresses the oxidation behavior of Co and yields the exsolution of Co-rich Ni–Co alloy nanoparticles during DRM.
- *Influence of the B' site cation:* We also reveal a strong response of molybdenum as the B' site cation to reduction and DRM treatment, causing the formation of reduced Mo species accompanying the exsolution process, which can be regarded as markers of increasing oxygen anion vacancy levels.

Double perovskites structures are, therefore, perfect model systems to monitor and classify the structural and electronic interactions potentially occurring in more complex oxide-based catalyst materials, and future studies must aim at a systematic exploration of the compositional parameter space of this material class by in-situ and operando techniques to enable a more rational knowledge-based catalyst design.

## CRediT authorship contribution statement

**Thomas F. Winterstein:** Methodology, Investigation, Formal analysis, Data curation. **Christoph Malleier:** Methodology, Investigation, Formal analysis, Data curation. **Bernhard Klötzer:** Writing – review & editing, Validation, Supervision, Conceptualization. **Volker Kahlenberg:** Writing – review & editing, Validation, Supervision, Project administration, Formal analysis, Conceptualization. **Clivia Hejny:** Writing – review & editing, Supervision, Formal analysis. **Maged F. Bekheet:** Writing – review & editing, Supervision, Formal analysis, Conceptualization. **Julian T. Müller:** Writing – review & editing, Funding acquisition. **Aleksander Gurlo:** Writing – review & editing, Funding acquisition. **Marc Heggen:** Writing – review & editing, Formal analysis, Data curation. **Simon Penner:** Writing – review & editing, Writing – original draft, Validation, Supervision, Project administration, Funding acquisition, Conceptualization.

## Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

## Data availability

Data will be made available on request.

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## Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.mtchem.2024.102255>.

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